

24 illite > chlorite > kaolinite. Subsequently, further investigation employing the developed TLM and
25 MEB revealed that higher amounts of kaolinite will make the reservoir more oil-wet.
26 Lastly, the sensitivity analysis performed on reservoir wettability indicated that the ionic
27 composition is the most important factor to affect rock wettability followed by pH and temperature.
28 Moreover, the presence of CaCl₂ salt in the formation water significantly suppresses the areas of
29 strong water wettability under varying reservoir conditions compared to NaCl salt.
30 The work conducted in this study presents a novel approach to model the individual and combined
31 effects of sandstone minerals, specifically, quartz, kaolinite, chlorite, illite, montmorillonite and
32 smectite, on the overall sandstone zeta potential behaviour. Furthermore, a new method was
33 proposed to characterise reservoir wettability as a function of the maximum energy barrier which
34 allowed us to obtain valuable insights into the most affecting reservoir parameters on COBR
35 wettability. These findings will have practical implications to efficiently design the low salinity
36 waterflooding processes for sandstone reservoir applications.

37 **Keywords:** *Rock-Brine Interface, Sandstone Reservoirs, Wettability Alteration, Triple-layer*
38 *Surface Complexation Modelling, Low Salinity Waterflooding*

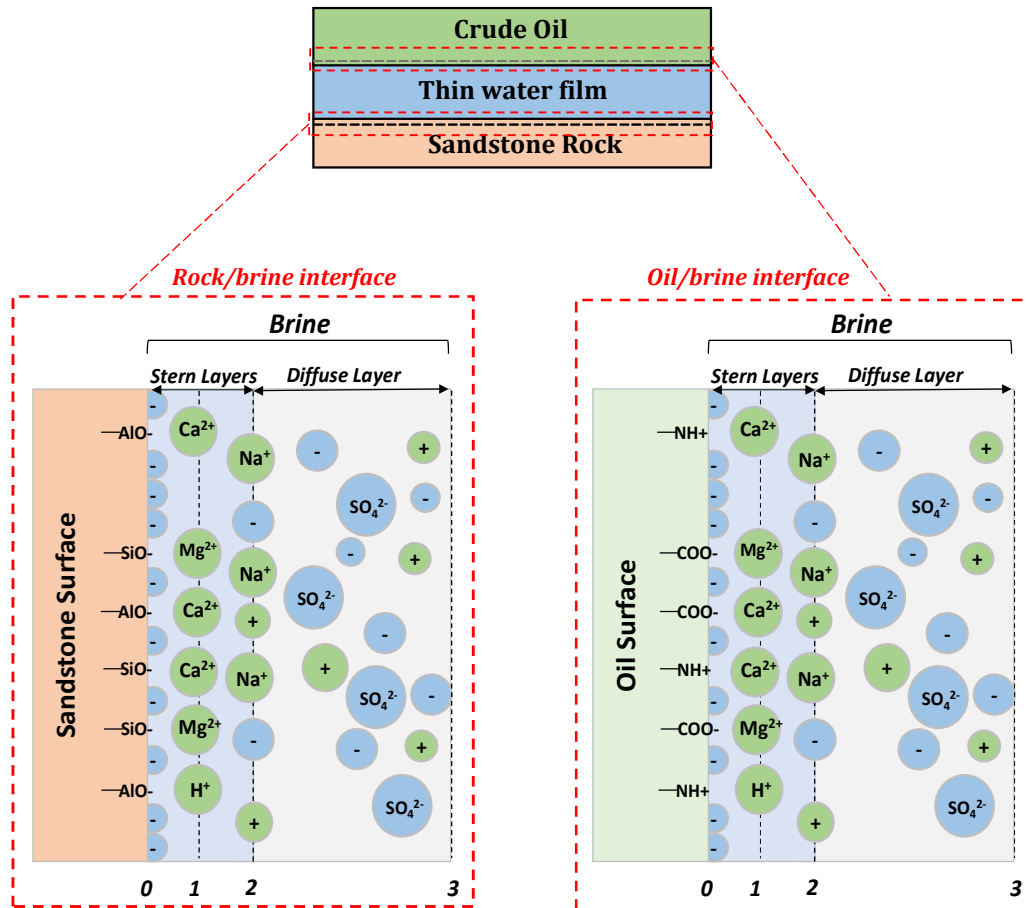
39 **2 Introduction**

40 Incremental oil recovery by low salinity waterflooding (LSWF) has been observed in both
41 experimental and field applications in the sandstone porous media and has been the focus of
42 numerous research studies [1]. LSWF has gained significant attention in the past two decades since
43 it is relatively cheap when compared to other conventional enhanced oil recovery technologies
44 (EOR) relying on costly chemicals and solvents. It also does not need major modifications in
45 producing facilities besides capitalizing on the waterflooding infrastructure already available in
46 sandstone oil fields. The synergization of LSWF with chemicals (surfactant, polymer) and
47 nanoparticles is also recently becoming popular due to the favourable effects of low salinity water
48 to reduce chemical usage and achieve higher oil recoveries [2-5].

49 Several mechanisms have been suggested to be the reason behind LSWF incremental recoveries
50 including the fines migration, multi-component ion exchange (MIE), double-layer expansion, and
51 alkaline-like effect [6-10]. There is no common consensus on a single mechanism, and it is also
52 most likely that a combination of these mechanisms may be in play depending on studied systems
53 and conditions. Double-layer expansion is widely believed to play an important role in bringing
54 out the favourable low salinity effect on changing the wettability of the porous medium via the
55 ionic interactions at the oil-brine and rock-brine interfaces. This paper presents the nano-scale
56 results of such interactions using a newly developed triple-layer surface complexation model
57 (TLM) in the crude oil-brine-rock system relevant to a sandstone reservoir. Wettability alteration
58 from oil-wet to water-wet conditions is believed to be a result of the double-layer expansion [11].
59 The charges at the oil-brine and rock-brine interfaces determine the thickness of thin water film
60 between the oil and rock surfaces. Negative charges at both interfaces cause them to repulse,
61 leading to the expansion of the thin water film thickness. Such expansion results in a more stable
62 colloidal crude oil-brine-rock system in sandstones, where the rock surface is in more contact with
63 brine than oil making the system water-wet. The interactions at the oil-brine and rock-brine
64 interfaces depend on the brine composition as well as the surface-active functional groups at the
65 oil and rock surfaces. The common surface-active groups on the oil surface are (-NH) and (-
66 COOH), and on the sandstone rock surface are (>AlOH) and (>SiOH). These surface groups
67 undergo protonation/deprotonation reactions and association/dissociation reactions with the
68 potential determining ions (PDIs) present in the brine, which determines the oil and rock surface
69 charges. More details on experimental evidence demonstrating how reservoir parameters dictate
70 the COBR interactions and low salinity waterflooding performance in sandstone rocks can be found
71 elsewhere [12].

72 Interactions at the oil-brine and rock-brine interfaces are simulated by the surface complexation
73 models (SCM). Brady and Krumhansl [13] highlighted that diffuse double-layer (DDL) SCM can

74 be used to calculate the concentration of the electrostatic bridges connecting the oil and clay
75 surfaces, thus predicting the degree of oil adhesion before and after the LSWF. The electrostatic
76 bridges [13] are a result of a series of chemical reactions and electro-kinetic attraction forces. The
77 COBR system in their model included rock containing kaolinite clay, oil with functional groups
78 carboxylic (-COOH) and nitrogen bases (-NH⁺) and divalent cations Ca²⁺ and Mg²⁺ in water. They
79 concluded that high concentrations of certain oppositely charged species such as [$> \text{Al}:\text{Si}-\text{O}^-$], [$>$
80 $\text{Al}-\text{O}-\text{H}_2^+$], [$-\text{COOCa}^+$], [$-\text{COO}^-$], [$-\text{NH}^+$] present on rock and oil surfaces, will lead to the
81 electrostatic attraction between the two surfaces resulting in the adhesion of oil to rock surface
82 (Figure 1). Details on the other oil-brine and rock-brine DDL-SCMs for both sandstone and
83 carbonate rocks have been reported elsewhere [14-21].



84

85 **Figure 1 (top) Representation of thin water film between oil/brine and rock/brine interfaces,**
 86 **(bottom) Representation of the sandstone-brine and oil-brine electrical interfacial layers**

87 On the other hand, triple-layer surface complexation models (TLMs) include three adsorption
 88 layers rather than two layers which is the case in double-layer models (see Figure 1). The layers in
 89 a TLM are the inner Helmholtz layer constrained by the electrostatic planes 0- and 1-planes, the
 90 outer Helmholtz layer between the 1- and 2-planes and the diffuse layer extending from the 2-plane
 91 to 3-plane. The inner and outer Helmholtz layers are known as the Stern layers as depicted in Figure
 92 1. Moreover, TLM enables the modelling of inner and outer Helmholtz layer complexes and the
 93 charge distribution of the adsorbed potential determining ions between the different electrostatic
 94 planes leading to a better representation of the electrical interfacial layers [22-24]. A few triple-
 95 layer surface complexation models (TLM) were developed to describe sandstone rock-brine
 96 interfaces [25-31]. Most of these previous TLMs used single minerals such as quartz and kaolinite

97 to describe the rock surface. However, the other clay minerals such as illite, chlorite, smectite,
98 montmorillonite, muscovite etc. are present in the sandstone and other clays. The individual and
99 combined effect of these other minerals on the overall surface charge and zeta potential in
100 sandstone rock systems were not accommodated in those investigated TLMs, which can be
101 considered as the most important limitation of previously reported models in the existing
102 knowledge.

103 The mineralogy of sandstone affects the wetting condition in the crude oil-brine-rock system
104 [11,13]. The sandstone rock surface chemistry is the resultant of the protonation/deprotonation and
105 cation/anion sorption reactions of the mineral surface groups. The clay surface charge can be
106 defined as the sum of the edge plane and basal plane charges. In this work, we consider only the
107 edge plane charge which is controlled mainly by the surface groups Aluminol ($>AlOH$) and Silanol
108 ($>SiOH$). In addition to the surface groups, clay surface charge is also dictated by the clay specific
109 surface area, temperature, brine salinity and pH [13,32]. Different clay minerals such as kaolinite,
110 illite and chlorite have different surface group site densities and specific surface areas. These
111 differences result in distinct surface charge behaviour for the individual clays and their overall
112 contribution to the sandstone rock surface charge [33,34].

113 In the present study, we build upon our findings from a previously published work [35] utilising
114 the newly developed oil-brine TLM, by integrating it with the sandstone-brine interfacial TLM
115 (this work) to evaluate the effect of different clay minerals. These clay minerals include kaolinite,
116 illite, chlorite, montmorillonite and smectite (in addition to quartz), which represent a considerable
117 portion of the overall sandstone rock mineralogy [36]. The values of the $>AlOH$ and $>SiOH$ surface
118 site densities and clay specific area for the modelled sandstone minerals were extracted from
119 various published experimental and modelling studies, as summarised in Table 1.

120 The novelty of work undertaken in this investigation lies in (i) the inclusion of the individual and
121 combined effects of different reservoir minerals, specifically quartz, kaolinite, chlorite, illite,

122 montmorillonite and smectite, on the surface charge behaviour at sandstone surface and (ii)
 123 development of the correlation between the maximum energy barrier, (defined as the maximum of
 124 the DLVO theory's interaction potential energy curve [37]) contact angles and reservoir wettability
 125 in different crude oil-brine-sandstone rock systems.

126 The following section will present the methodology adopted in this work. Subsequently, the results
 127 of sandstone-brine interface model validation and zeta potential sensitivity analysis are discussed.
 128 Later, wettability correlation with the maximum energy barrier parameter is presented followed by
 129 sensitivity analysis of COBR wettability to various reservoir parameters.

130 **Table 1 Specific surface area and surface site density for sandstone minerals modelled in this work**

Mineral	Specific surface area (g/m ²)		Surface site density (site/nm ²)		
	Value	Reference	>AlOH	>SiOH	Reference
Kaolinite	12	[38]	5.5	5.5	[33,38]
Chlorite	2.4	[38]	5.5	5.5	This study
Illite	22.3	[39]	≈2.6	≈5.3	[34]
Montmorillonite	71	[38]	≈1	≈2	[40]
Smectite	31	[41]	≈0.6	≈0.6	[41]
Quartz	0.426	[42]	-	10	[43]

131 **3 Methodology**

132 The methodology adopted to develop the triple-layer surface complexation model describing the
 133 sandstone-brine interfacial interactions is presented. The developed sandstone-brine TLM was then
 134 validated and employed to assess the impact of rock mineralogy, salinity, and pH on the rock-brine
 135 zeta potential. The validated sandstone-brine interface model is further integrated with our
 136 previously reported oil-brine TLM [35] and the Derjaguin, Landau, Verwey, and Overbeek
 137 (DLVO) theory [44] to understand film stability and reservoir wettability alteration during the
 138 LSWF.

139 **3.1 Sandstone Rock-Brine Triple-Layer Surface Complexation Model (TLM)**

140 A sandstone rock-brine TLM was developed using the Donnan approach in CD-MUSIC, a module
141 of the geochemical code PHREEQCTM [45]. This TLM simulates the interactions at the rock-brine
142 interface while taking account of the following parameters: inner and outer-Helmholtz layer
143 capacitances, protonation/deprotonation and association/dissociation reactions equilibrium
144 constants, surface site densities, specific surface areas and charge distribution. The assumptions
145 made during this TLM development were: (i) quartz, kaolinite, illite, chlorite, montmorillonite and
146 smectite are the most abundant minerals in the sandstone reservoir, hence their individual
147 behaviour governs the overall sandstone surface charge behaviour; (ii) the overall average
148 behaviour can be predicted by weight-averaging the specific surface area and surface site densities
149 for each mineral; and (iii) the surface site density of chlorite is same as kaolinite due to a lack of
150 data in the published literature. The results obtained from triple-layer modelling were validated
151 against the reported experimental data (see Table 2) available in the literature.

152 **Table 2 Summary of experimental conditions used for the published zeta potential data**
 153 **at the sandstone-brine interface**

Reference	Rock Sample	Brine Electrolyte	Brine Salinity	pH	Temperature (°C)
[46]	Berea Sandstone	NaCl, CaCl ₂	1500 ppm	2 to 11	25
[47]	Sandstone	NaCl, CaCl ₂ , MgCl ₂	0.1 - 5 wt.%	7.3 to 9	25
[48]	Kaolinite, Montmorillonite	NaCl, CaCl ₂	0.05 - 0.3 wt%	6.05 to 6.83	Room Temperature
[49]	Kaolinite	CaCl ₂ , MgCl ₂	50 - 500 mmol/L	1.8 to 7.8	25
[50]	Sandstone	NaCl	0.2 - 10 wt.%	7.1 to 8.4	65
[51]	Berea Sandstone, Scioto Sandstone	Deionized Water, Aquifer Water, Seawater	5,436 - 174,156 mg/L	7.29 to 7.84	25
[52]	Kaolinite	NaCl	0.02 mol/L	3 to 11	25
[53]	Kaolinite	NaCl	0.0001 - 0.01 mol/L	3 to 11	25

154
 155 The surface groups of minerals used are Aluminol (>AlOH) and Silanol (>SiOH). The potential
 156 determining ions (PDIs) modelled in the brine are calcium, magnesium, sodium, hydroxyl and
 157 hydrogen ions. The effect of sulphate ions in brine on zeta potential at the rock-brine interface is
 158 also evaluated in the model. The sodium ion forms an outer-sphere complex with the surface groups
 159 (>Al:SiOH) with its charge distributed between the 1- and 2-planes, while the calcium and
 160 magnesium ions form inner-sphere complexes with (>Al:SiOH) and have their charges on the 1-
 161 plane [23,54].
 162 For pure individual clay minerals, the values of specific surface areas and surface site densities for
 163 >Al:SiOH, reported in Table 1, were directly used in the model to evaluate the rock-brine
 164 interactions. In modelling the surface of a sandstone rock comprising multiple minerals, the

165 weighted-average values of the surface site densities and specific surface area were employed. The
 166 specific surface area (SSA_{avg}) used in the model was averaged by the mineral weight/volume % in
 167 the overall sandstone rock mineralogy as shown in Eq. (1)

$$SSA_{avg} = \sum_i SSA_i \times wt_i\%(or\ vol_i\%) \quad \text{Eq. 1}$$

168 where SSA is the specific surface area and i denotes the mineral type. The surface site densities
 169 (N_s) for $>AlOH$ and $>SiOH$ were averaged based on both mineral weight/volume % in the overall
 170 sandstone rock mineralogy and the specific surface area of each mineral, using the following
 171 equation:

$$N_{s,avg} = \frac{\sum_i N_{s,i} \times SSA_i \times wt_i\%(or\ vol_i\%)}{SSA_{avg}} \quad \text{Eq. 2}$$

172 The capacitances (see Table 3) of the inner and outer Helmholtz layers determine the potential drop
 173 across the layer. These are dependent on the dielectric constant of the electrolyte and the distance
 174 between the planes. The detailed procedure for calculating the capacitance for each layer can be
 175 found in Saeed et al. [35]. The thickness of the diffuse layer was assumed to be twice the screening
 176 Debye length [34]. The inverse Debye length is calculated as follows:

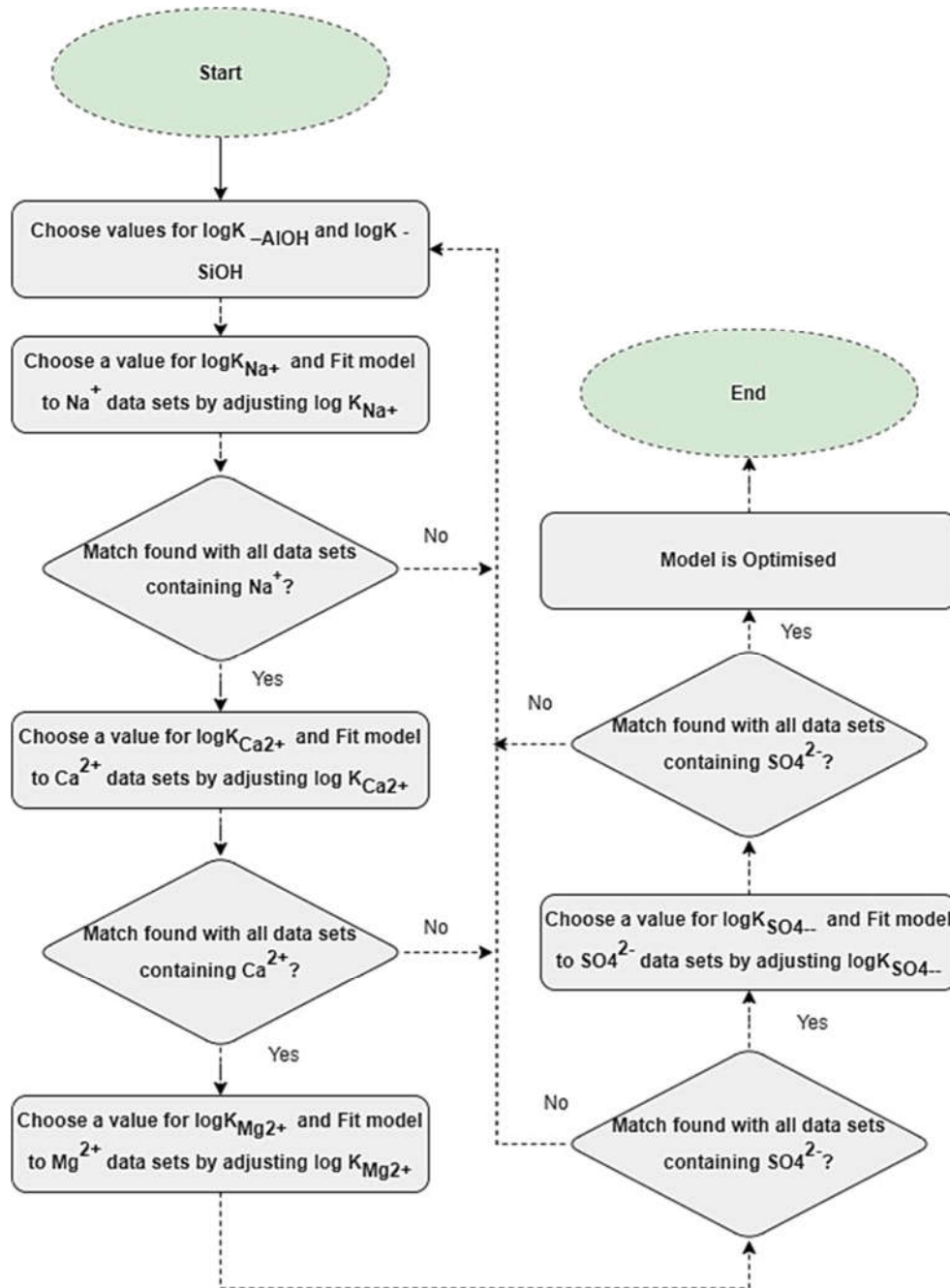
$$k^{-1} = \sqrt{\frac{\epsilon_0 \epsilon_r k_B T}{2000 N_A e^2 I}} \quad \text{Eq. 3}$$

177 where k_B is the Boltzmann constant, T is the absolute temperature, N_A is Avogadro's number, e is
 178 the electron charge, and I is the ionic strength of the solution.

179 3.1.1 Optimization of the sandstone Rock-Brine TLM

180 The association/disassociation equilibrium constants of the surface groups, $>AlOH$ and $>SiOH$,
 181 were optimized to converge between the modelling and experimental zeta potential values. The
 182 modelling optimization process, illustrated in Figure 2, follows the optimization process described
 183 by Saeed et al. [35]. The experimental data required for the modelling run are brine composition,
 184 pH, temperature and sandstone rock mineralogy to calculate the average specific surface area for

185 the rock and average surface site densities of >AlOH and >SiOH. The optimized surface
 186 complexation reactions constants are shown in Table 3 along with the reactions' enthalpy, the
 187 charge distribution of the modelled PDIs and the capacitances of the inner and outer Helmholtz
 188 layers.



189
 190
 191 **Figure 2 Sandstone rock-brine TLM optimization process flowchart**

192

193 **Table 3 Association/disassociation equilibrium constants, charge distribution and capacitance values**
 194 **optimised in this study for the developed sandstone-brine TLM**

Surface Complexation Reaction	Log K @ 25° C	Enthalpy (kJ/mol)	Charge Distribution			C ₁ (F/m ²)	C ₂ (F/m ²)
			0-plane	1-plane	2-plane		
$>AlOH + H^+ \leftrightarrow >AlOH_2^+$	0.8	-5	+1	0	0	2.57	2.57
$>AlOH \leftrightarrow >AlO^- + H^+$	-7.5	-40	-1	0	0	2.57	2.57
$>AlOH + Na^+ \leftrightarrow >AlONa + H^+$	-4.5	-60	-1	+0.5	+0.5	2.57	2.57
$>AlOH + Ca^{2+} \leftrightarrow >AlOCa^+ + H^+$	-3.5	-50	-1	+2	0	3.54	2.57
$>AlOH + Mg^{2+} \leftrightarrow >AlOMg^+ + H^+$	-3.5	-50	-1	+2	0	4.92	2.57
$>AlOH + SO_4^{2-} \leftrightarrow >AlO^- + HSO_4^-$	-1.5	-	-1	0	0	2.57	2.57
$>SiOH \leftrightarrow >SiO^- + H^+$	-6.5	-40	-1	0	0	2.57	2.57
$>SiOH + Na^+ \leftrightarrow >SiONa + H^+$	-2	-60	-1	+0.5	+0.5	2.57	2.57
$>SiOH + Ca^{2+} \leftrightarrow >SiOCa^+ + H^+$	-2.5	-50	-1	+2	0	3.54	2.57
$>SiOH + Mg^{2+} \leftrightarrow >SiOMg^+ + H^+$	-2.8	-50	-1	+2	0	4.92	2.57
$>SiOH + SO_4^{2-} \leftrightarrow >SiO^- + HSO_4^-$	-1.5	-	-1	0	0	2.57	2.57

195
 196 The sandstone-brine TLM developed in this study overcomes the limitations of previously reported
 197 sandstone rock-brine SCMs and TLMs [25-31]. The developed TLM successfully incorporates the
 198 individual and combined effects of the most abundant clays and minerals present in sandstone
 199 rocks, thereby providing an improved ability to quantify the impact of each clay on the overall zeta
 200 potential and reservoir wettability. The model was found to be effective in describing the adsorption
 201 of various PDIs i.e. H⁺, Na⁺, Ca²⁺ and Mg²⁺, on the inner and outer Helmholtz layers of the
 202 sandstone rock-brine interface. The model also describes the effect of sulphate ions present in brine
 203 on the sandstone rock-brine interface.

204 3.2 Oil-brine interface TLM

205 Our previously reported oil-brine TLM [35] is integrated with the sandstone-brine TLM developed
206 in this study, to evaluate the complete Crude Oil Brine Rock (COBR) system. The stability of the
207 COBR was characterised using the DLVO theory calculations. The association/disassociation
208 reaction equilibrium constants, charge distribution and capacitance were also considered in this
209 study. The oil-brine TLM incorporates the effects of both the acidic and basic groups i.e. (-COOH)
210 and (-NH), on the oil surface, and the adsorption/desorption of the PDIs, Na⁺, Ca²⁺, Mg²⁺ and H⁺,
211 on the oil surface groups. More details on the adopted oil-brine TLM can be found in [35].

212 3.3 Disjoining Pressure Calculations and Film Stability

213 The crude oil-brine-rock (COBR) system is analysed by calculating the disjoining pressure using
214 the DLVO theory. The calculation of disjoining pressure requires the knowledge of zeta potentials
215 at the oil-brine and rock-brine interfaces. These zeta potential values are adapted from the
216 simulation output of the developed TLM and the geochemical code PHREEQC. The disjoining
217 pressure can be calculated as the sum of two repulsive forces and an attractive force. The two
218 repulsive forces are the electrical double-layer force and the structural force, while the attractive
219 force is the Van der Waals force. To calculate the disjoining pressure, the individual forces are
220 calculated and added together to find the net force acting between the oil-brine and rock-brine
221 interfaces.

$$\Pi(h) = \Pi_{vdw}(h) + \Pi_{structural}(h) + \Pi_{electric}(h) \quad Eq 4$$

222 The Van der Waals forces between two plates including the retardation effects are calculated
223 according to the following formula [55]:

$$\Pi_{vdw}(h) = -\frac{A \left(15.96 \left(\frac{h}{\lambda_{lw}}\right) + 2\right)}{12\pi h^3 \left(1 + 5.32 \left(\frac{h}{\lambda_{lw}}\right)\right)^2} \quad Eq 5$$

224 where, λ_{lw} is the London wavelength and is assumed to be 100 nm [55], h is the distance between
 225 the two interfaces and A is the Hamaker constant, obtained through [44]:

$$A = A_{v=0}(\kappa h)\exp(-2\kappa h) + A_{v>0} \quad Eq\ 6$$

226 where κ is the Debye-Huckel parameter, $A_{v=0}$ and $A_{v>0}$ are the contributions to Hamaker constant
 227 at zero and finite frequencies, respectively obtained using the following equations [44]:

$$A_{v=0} = \frac{3}{4}kT \left(\frac{\varepsilon_1 - \varepsilon_3}{\varepsilon_1 + \varepsilon_3} \right) \left(\frac{\varepsilon_2 - \varepsilon_3}{\varepsilon_2 + \varepsilon_3} \right) \quad Eq\ 7$$

$$A_{v>0} \approx \frac{3h\nu_e}{8\sqrt{2}} \frac{(n_1^2 - n_3^2)(n_2^2 - n_3^2)}{(n_1^2 + n_3^2)^{0.5}(n_2^2 + n_3^2)^{0.5}\{(n_1^2 + n_3^2)^{0.5} + (n_2^2 + n_3^2)^{0.5}\}} \quad Eq\ 8$$

228
 229 where ε_1 , ε_2 and ε_3 are the dielectric constants for medium 1, 2 and 3, as considered in our case for
 230 hydrocarbons, quartz and water, respectively. n_1 , n_2 and n_3 are the refractive indexes for medium
 231 1, 2 and 3, respectively. The values for these parameters to calculate the Hamaker constant can be
 232 found in [44]. The structural forces are effective at low separation distances between the two
 233 interfaces < 5 nm [56] and are calculated as follows:

$$\Pi_{structural}(h) = A_s e^{-\frac{h}{h_s}} \quad Eq\ 9$$

234 where A_s is a coefficient, assumed to be 1.5×10^{10} Pa [37] and h_s is the characteristic length,
 235 assigned the value of 0.05 nm [37].

236 For the two charged surfaces approaching each other, the two solutions for the Poisson-Boltzmann
 237 equation can be obtained using two different conditions [37,55,57]. One solution is the constant
 238 potential solution, and the other is the constant capacitance charge. It is predicted that a solution
 239 between them occurs. In this work, it is assumed that a constant potential solution [58] applies to
 240 simplify our calculations. Hence, the force resulting from the interaction of the two charged
 241 surfaces of oil and sandstone can be calculated by

$$\Pi_{electric}(h) = n_b k_b T \left(\frac{2\psi_{r1}\psi_{r2} \cosh(\kappa h) - \psi_{r1}^2 - \psi_{r2}^2}{[\sinh(\kappa h)]^2} \right) \quad Eq 10$$

242 where n_b is the ion density in the bulk solution, k_b is the Boltzmann constant (1.38×10^{-23} J/K), ψ_{r1}
 243 and ψ_{r2} are the reduced surface potentials for the rock-brine and oil-brine interfaces, respectively,
 244 and κ is the Debye-Hückel reciprocal length. The reduced potential can be calculated as follows:

$$\psi_r = \frac{ze\zeta}{kT} \quad Eq 11$$

245 where ζ is the zeta potential at the interface of interest. The specific interaction potential energy
 246 between two phases interacting through a third phase can be calculated as follows [37]

$$\omega = \int_h^{h_{eq}} (\Pi - \Pi_{eq}) \cdot dh \quad Eq 12$$

247 where h_{eq} and Π_{eq} are the separation distance and disjoining pressure at equilibrium conditions. The
 248 stability of the COBR system is directly related to the maximum interaction potential energy barrier
 249 (MEB), below which the VdW forces become dominant and the colloid falls into an unstable region
 250 and is destroyed [559].

251 In this work, we propose the use of MEB as the main indicator for film stability, and hence the
 252 wettability of the reservoir under investigation. The maximum energy barrier is calculated as the
 253 maximum of the interaction potential curve. To understand the effects of various reservoir
 254 parameters on the oil-brine-sandstone rock system's stability and wettability, the MEB is evaluated
 255 for several cases by varying the studied reservoir parameters. The MEB is calculated at zero
 256 capillary pressure in all the studied cases. Capillary pressure does affect the reservoir's wettability,
 257 however, setting its value to zero eliminates its effects on wettability and therefore focuses the
 258 investigation on the basis of brine, oil and rock compositions, pH and temperature only. For this
 259 application, we observe that the maximum energy barrier for the modelled cases ranges at film
 260 thicknesses between 0.5 and 1.5 nm. Hence, for consistency, we calculate the maximum of the
 261 interaction potential at this range for all the studied cases. With a higher MEB, the oil-brine-

262 sandstone system is more stable, and thus more water wet. As the MEB decreases, the stability of
263 the oil-brine-sandstone system becomes less stable and less water-wet. The factors affecting the
264 oil-brine-sandstone system's wettability include pH, temperature, salinity, oil TAN and TBN, and
265 rock mineralogy among others. The first step in calculating the interaction potential energy is to
266 model the oil-brine and rock-brine zeta potentials. The disjoining pressure is calculated according
267 to *Eq 4*. Interaction potential is calculated using *Eq 12*. Finally, sensitivity analysis was utilised to
268 evaluate the sensitivity of COBR wettability to changes in oil TAN and TBN, sandstone rock's
269 average rock site density, brine composition, pH and temperature. This eventually enabled us to
270 produce wettability maps for NaCl and CaCl₂ systems to further understand the importance of each
271 parameter on wettability determination during the low salinity waterflooding process in sandstone
272 reservoirs.

273 **4 Results and Discussion**

274 The published data sets of zeta potential measurements using brines and sandstone rock (see Table
275 2) were first extracted and then used to calibrate and validate the developed triple-layer model
276 (TLM). The extracted datasets composed of experimental results performed under varying brines,
277 sandstone mineralogical composition, pH, and temperatures. The correlation analysis between the
278 calculated MEB and experimentally measured contact angles was performed. Results of sensitivity
279 analysis are reported and discussed to evaluate the importance of the various parameters in dictating
280 the zeta potential of a sandstone-brine interface and the sandstone reservoir wettability.

281 **4.1 Sandstone-brine Triple-layer Model Validation**

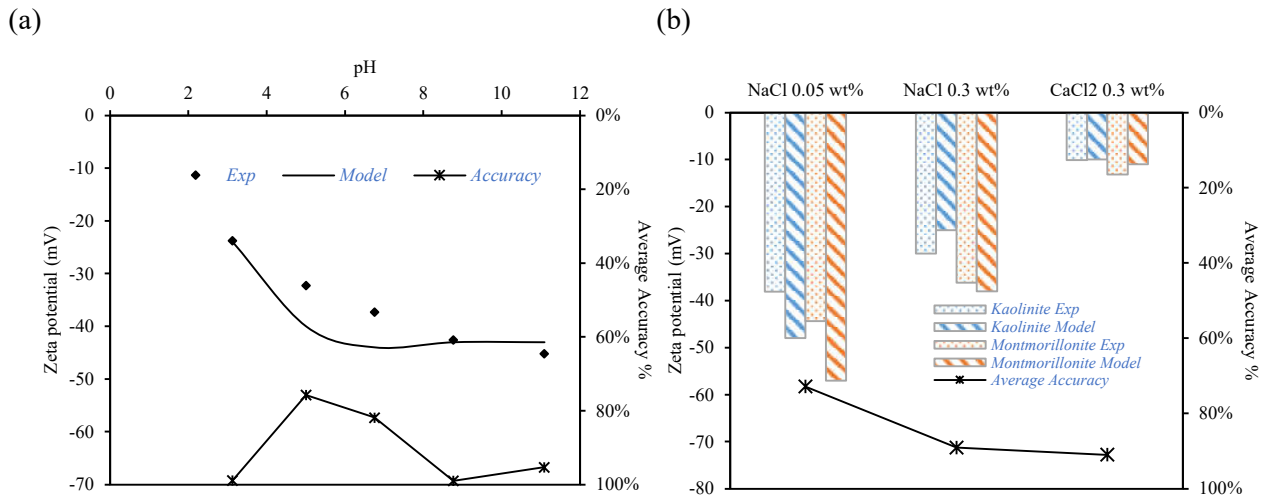
282 The developed model is validated, against the experimental datasets as detailed in Table 2. The
283 validation was carried out by comparing the experimentally measured zeta potential with the
284 model-predicted zeta potential values.

285 4.1.1 *Modelling the zeta potential of pure clays*

286 The experimental data from Yukselen-Aksoy and Kaya [52] were used to validate and calibrate the
287 model developed in this work. Yukselen-Aksoy and Kaya used kaolinite as the rock sample and
288 NaCl as the background electrolyte with a concentration of 0.02 M NaCl. The zeta potential was
289 predicted for a pH range of 3 to 11 and at 25 °C temperature. The TLM simulation results (Figure
290 3) display the capability of the model to predict the trend of the zeta potential change with pH in
291 the studied range. The results indicate that an increase in the pH value leads to higher negative zeta
292 potential values which can be attributed to the enhancement of Al:SiOH deprotonation. This
293 deprotonation causes the increase of the negatively charged Al:SiO⁻ surface groups which
294 progressively charge the kaolinite surface with a negative charge. The values of zeta potential
295 calculated by the TLM were in close agreement with the experimental values except at pH between
296 5.0-6.8 where discrepancies are apparent, and the accuracy of the model drops to the range 76% -
297 82% which highlights some slight inaccuracy in modelling.

298 The effect of NaCl and CaCl₂ electrolyte on the zeta potential at the pure clay-brine surface was
299 evaluated in this study using the experimental data extracted from Bazyari et al. [48]. The TLM
300 was used to predict the zeta potential values at the rock-brine interface for two different types of
301 pure clay minerals - kaolinite and montmorillonite. The TLM predicted results are matched with
302 the experimental results reported [48] (see Figure 3). The model was able to closely predict the zeta
303 potential values. It can also be seen that CaCl₂ electrolytes caused the zeta potential to be less
304 positive for both kaolinite and montmorillonite in contrast to the NaCl electrolyte effect. This is
305 attributed to the presence of the divalent cation Ca²⁺ which causes higher electrical screening to the
306 negative charge present on the clay surfaces. The model shows accuracy ranging between 73% and
307 91% for the studied cases. The model exhibits better accuracy in predicting zeta potential in higher
308 ionic strength electrolytes. This can be explained by the fact that higher ionic strength leads to

309 suppressing the zeta potential values, thereby minimising the discrepancies between model and
 310 measured zeta potentials.



311
 312 **Figure 3 Experimental and modelling zeta potential values for (Left) Kaolinite [52] and (Right)**
 313 **kaolinite and montmorillonite [53]**

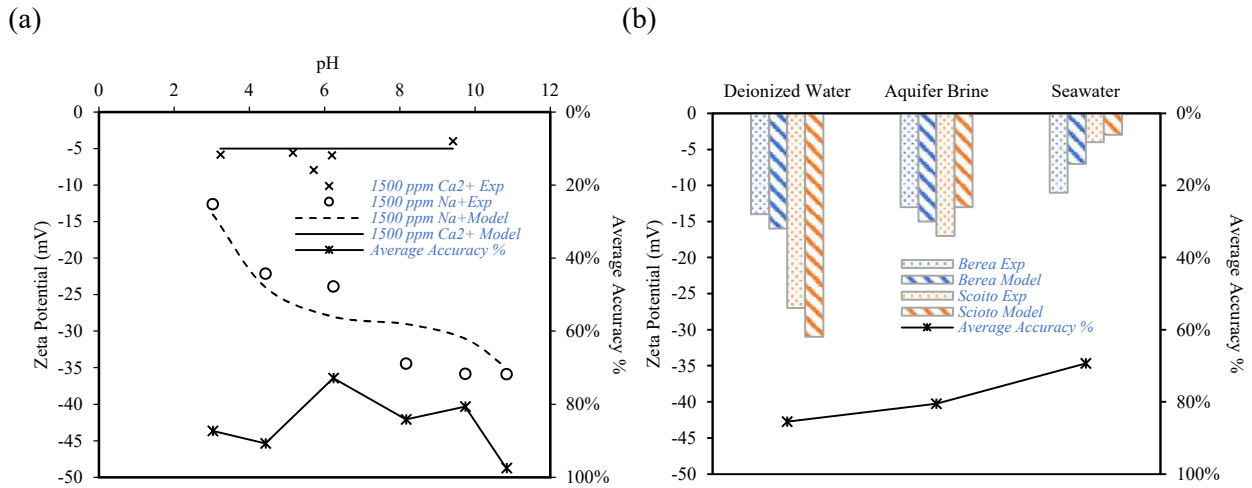
314 *4.1.2 Modelling the zeta potential of sandstone rocks*

315 The rock-brine TLM proposed in our work was also used to replicate the experimental results of
 316 Farooq et al. [46] who studied the effect of varying cationic valences and pH conditions on an
 317 outcrop Berea sandstone sample. All their experiments were conducted at 25°C temperature
 318 conditions. The Berea sandstone sample mineralogy was used to calculate the rock properties
 319 required as input parameters of the TLM: average >Al:SiOH site density and average specific
 320 surface area using Eq. 1 and Eq. 2. Then the model was run to predict the zeta potential of the two
 321 cases using 1500 ppm and 1500 ppm electrolyte concentrations of NaCl and CaCl₂, respectively.
 322 The capacitance of the first layer parameter was varied according to the type of electrolyte used,
 323 2.57 and 3.54 F/m² for NaCl and CaCl₂ in that order. For all cases, the second layer capacitance
 324 was fixed at a value of 2.57 F/m².

325 The model results and their comparison with the experimentally reported zeta potentials are shown
 326 in Figure 4a. The model successfully predicts the zeta potential for the Berea sandstone sample

327 within close proximity in both NaCl and CaCl₂ electrolytes. In addition, the model also provided
328 accurate zeta potential predictions at high and low pH values with only small discrepancies at
329 higher pH values. The model accuracy ranged between the average 73% and 97% averaged for
330 both electrolytes containing Na⁺ and Ca²⁺ respectively.

331 The developed sandstone-brine model was also tested against its ability to capture the effect of
332 various clays present in the sandstone rock sample. Alotaibi et al. [51] focused on using Berea and
333 Scioto sandstone samples in different electrolytes including deionized water, aquifer water and
334 seawater. The salinity of the different electrolytes in addition to the mineralogy of the two rock
335 samples were used in the developed model to calculate the zeta potential. Figure 4b presents both
336 the experimental and modelling results as calculated from the TLM. The results demonstrate the
337 ability of the model to give an accurate prediction of the zeta potential for both Berea and Scioto
338 sandstone (Figure 4b) in deionized water and aquifer water with accuracies of 85% and 81%,
339 respectively. However, there is distortion in modelling the seawater experiments which can be
340 attributed to its considerably higher concentration of ions, and the different types of ions that are
341 not included in this model. This has led the model to have a lower accuracy of about 70%. It is
342 expected that incorporating the adsorption of more ions on the inner and outer Helmholtz layers
343 would increase the model accuracy, especially in such cases where seawater is used as an
344 electrolyte.

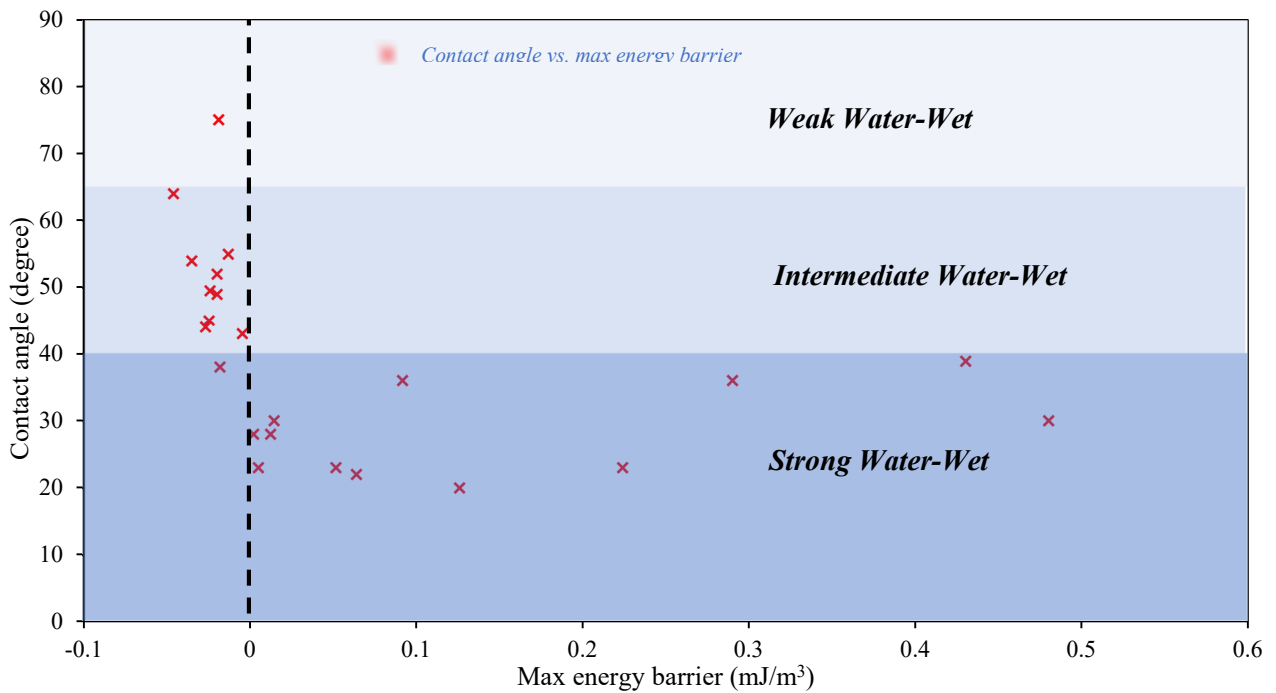


345
346 **Figure 4 Experimental and modelling zeta potential values for (a) Berea sandstone [46] and (b)**
347 **Berea sandstone sample and Scioto sandstone sample [51]**

348 4.2 Wettability, film stability and the maximum energy barrier

349 First, we test the hypothesis that the maximum energy barrier is an indicator of reservoir wettability.
350 The maximum of the interaction potential curve was calculated for several published experimental
351 datasets [11, 17, 50, 59 – 61] obtained using different sandstone samples, reservoir minerals, oil
352 composition, brine composition and temperature conditions. The MEB values was calculated from
353 the zeta potential measurements reported in these published experimental datasets. The results were
354 then fitted with the measured contact angles, as shown in Figure 5. Reservoir wettability is defined
355 by the contact angle with the range 0° to 40° being strong water-wet, 40° to 65° as intermediate
356 water-wet and 65° to 90° as weak water-wet. Figure 5 shows that as the MEB decreases from 0.07
357 to zero, the contact angle increases from 20° to 32°. However, this increase in the contact angle is
358 sharper when MEB goes into negative. Such observation indicates that a small reduction in the
359 MEB below zero-value increases the contact angle sharply, thereby causing the system to become
360 less water wet (intermediate water-wet). The data depicted in Figure 5 clearly show two trends, one
361 below zero MEB where the reservoir wettability abruptly becomes weaker with the decrease in the

362 MEB. While above zero MEB, the reservoir tends to stay in the strong water-wet region. These
363 results validate our hypothesis that the MEB can be used as an indicator of reservoir wettability.



364
365 **Figure 5 Correlation between experimentally measured contact angles and calculated maximum**
366 **energy barrier for each contact angle [11, 17, 50, 59 – 61]**

367 4.3 Effect of clay minerals on zeta potential and maximum energy barrier

368 Using the optimized modelling parameters of the different clay minerals shown in Table 1 and
369 Table 3, the model was further employed to understand and compare the effects of the individual
370 clay minerals on zeta potential at the rock-brine interface. The model was run for each individual
371 clay under the same conditions. The zeta potential curve for the five clay minerals under study is
372 plotted against the system pH (Figure 6). The results show that smectite, montmorillonite and
373 chlorite result in more negative zeta potential values with smectite having the highest negative zeta
374 potential within the studied conditions. The effect of kaolinite on zeta potential is lower compared
375 to the other three clays. Similar trend is observed for both 0.05 M NaCl (Figure 6a) and 0.005 M
376 NaCl (Figure 6b) electrolytes. The order by which the clays affect the zeta potential is directly
377 correlated with the site density of the surface species at clays. From Table 1, the site density at

378 >Al:SiOH surface for kaolinite and smectite is 11 site/nm² and 1.2 site/nm² respectively. If we
379 compare the zeta potential curves for kaolinite and smectite in Figure 6, it is evident that in the case
380 of kaolinite the zeta potential values are less negative than those of the smectite case. This can be
381 attributed to the higher presence of >Al:SiOH sites on the kaolinite mineral compared to smectite,
382 leading to a more negatively charged >Al:SiO⁻. These are the possible sites where the positively
383 charged Na⁺ can adsorb to. This adsorption leads to the screening of the surface charge present on
384 the clay surface. Hence, the higher the presence of clay minerals in the sandstone rock, especially
385 kaolinite, the more the zeta potential values at the sandstone rock-brine interface tend to be less
386 negative. The experimental results published in [38,48] are in line with our findings. Mahani et al.
387 [62] also highlighted that clays act as pinning points to crude oil which supports the results obtained
388 in this study. Montmorillonite clay exhibited higher negative zeta potential values in comparison
389 with kaolinite clay. Other studies [47,63,64] reported that the montmorillonite clay had higher
390 negative zeta potential than kaolinite, illite and chlorite in electrolytes with different ionic strengths
391 and over a wide range of pH. Our finding that the montmorillonite clay leads to negative zeta
392 potential values higher than kaolinite, chlorite and illite also agrees with the published experimental
393 results. Da Costa et al [65] measured the zeta potential for three types of sandstone: Botucatu, Berea
394 and Bentheimer, in various electrolyte ionic strengths. Zeta potential curve shifted towards more
395 negative values as the clay content in the sandstone rock decreased. Hence, the Bentheimer
396 sandstone had a zeta potential curve that is more negative than the Berea sandstone, which is more
397 negative than the Botucatu sample, exemplifying an important role of clays, as concluded in our
398 work.

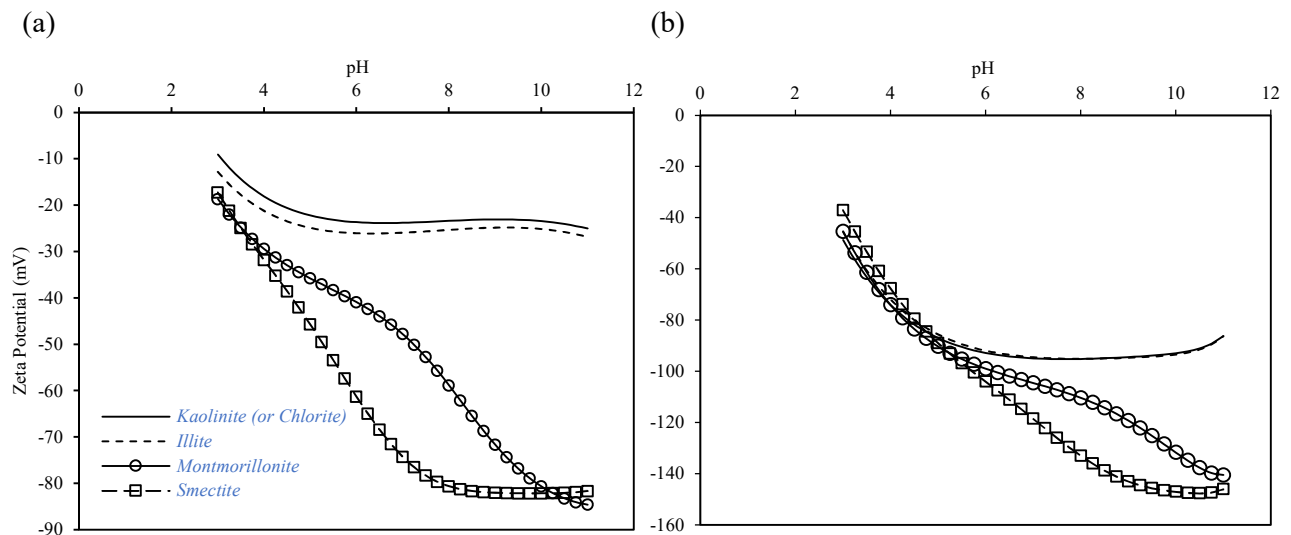


Figure 6 Zeta potential curves for different clay minerals in (a) 0.05 M NaCl electrolyte and (b) 0.005 M NaCl electrolyte

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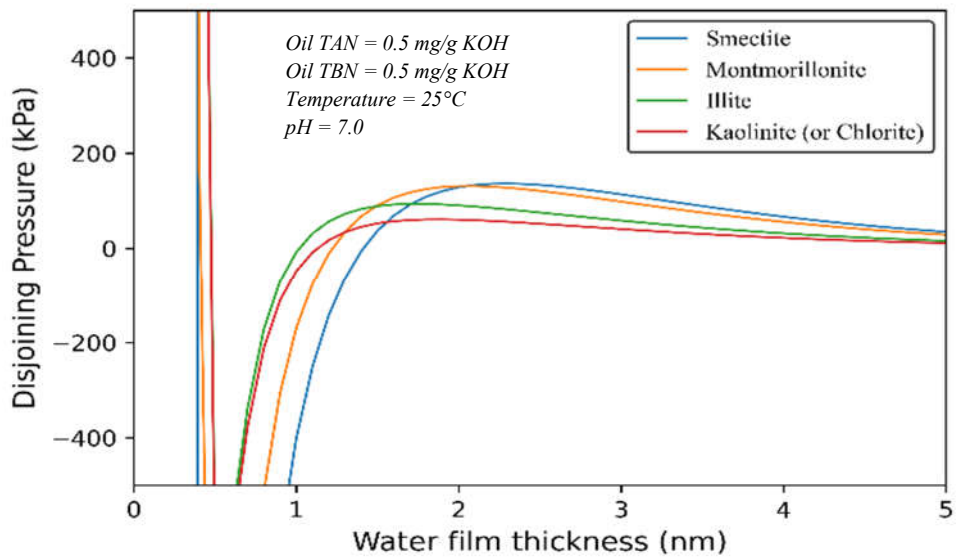
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The $>Al:SiOH$ surface site densities used are the averaged $>AlOH$ and $>SiOH$ site densities based on the mineral contents of the sandstone rock in question. The average $>Al:SiOH$ surface site density affects the overall stability of the COBR system via the zeta potential at the rock-brine interface. More the negatively charged $>Al:SiO^-$, higher will be the site density (where the cations can adsorb to), hence a less negative zeta potential at the rock-brine interface. This will lead to a lower overall disjoining pressure and interaction potential as shown in Figure 7. The results depicted in Figure 7 are in line with the findings of Bazyari et al [48] to confirm that montmorillonite exhibits disjoining pressure higher than kaolinite for several background electrolytes over a wide range of water film thickness. Based on these analyses and the MEB calculated for each clay (see Figure 8), it is concluded that the clays investigated in this study cause the zeta potential to be more negative and hence the COBR system more stable in the following order: smectite $>$ montmorillonite $>$ illite $>$ chlorite $>$ kaolinite. This implies that the higher the presence of clays that have higher $>Al:SiOH$ site density such as kaolinite, the lower the stability of the COBR system. Borysenko et al. [66] measured the air/water contact angles of kaolinite and montmorillonite. They found that the montmorillonite clays had lower contact angles than kaolinite

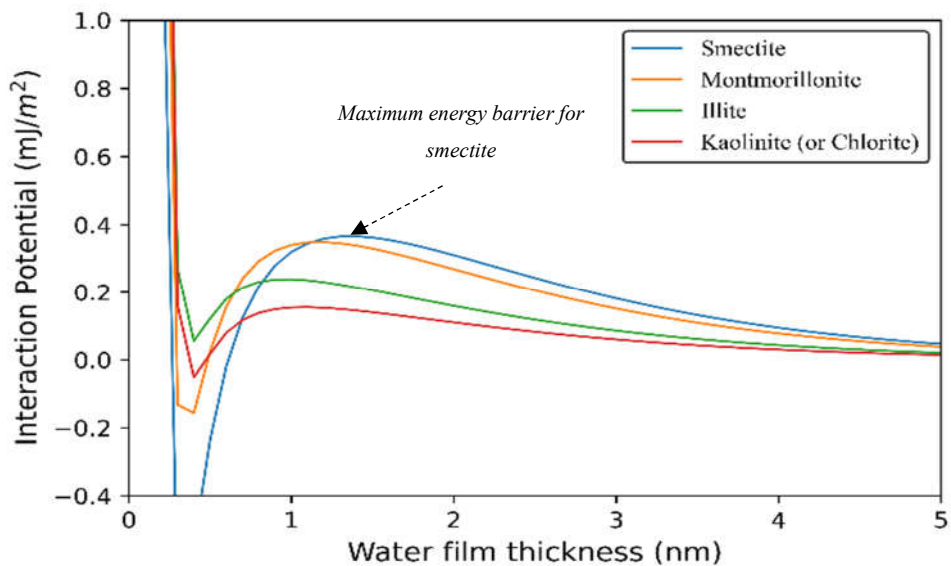
417 clays, which is in line with the MEB results depicted in Figure 8. The rapid change in the maximum
418 energy curve with the average rock site density demonstrates the significance of the sandstone rock
419 mineralogy in dictating the wettability of the oil-brine-rock system.

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(a)

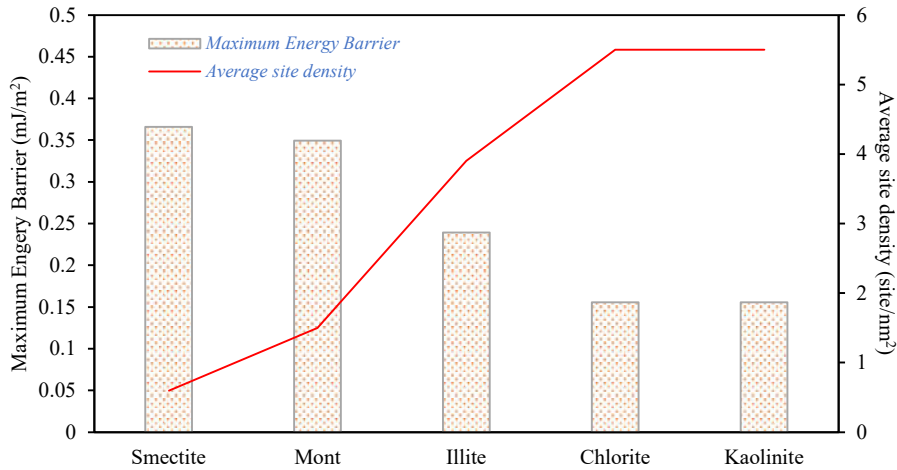


(b)



421

422 **Figure 7 (a) Disjoining pressure and (b) interaction potential curves for oil-brine and rock-brine**
 423 **interfaces with various clay minerals**



424
 425 **Figure 8 Maximum energy barrier variation with clay mineral type and average rock site density**

426 4.4 Sensitivity of energy barrier to reservoir conditions and composition

427 Sensitivity analyses were performed to understand the contribution of various parameters in the
 428 overall stability and wettability of the COBR system. These sensitivity analyses were carried out
 429 using the workflow developed in this study, including predicting the zeta potential values using the
 430 developed TLMs followed by calculating the disjoining pressure and interaction potential energy
 431 for each studied case. Finally, the MEB was determined from the calculated interaction potential
 432 energy curves. The studied parameters include brine ionic strength, pH, temperature, rock
 433 mineralogy, oil TAN and oil TBN. The analysis was carried out by determining a base case value
 434 for each parameter, as well as minimum and maximum values to simulate the reservoir conditions
 435 of potential interest (see Table 4). Then each parameter was allowed to be changed in isolation
 436 from the other parameters between its minimum and maximum values, which allowed us to
 437 quantify the individual impact of each parameter within the studied range. The results of the
 438 sensitivity analyses are presented in Figure 9. From Figure 9, it can be clearly seen that the most
 439 important parameters that affect the reservoir wettability are the ionic strength, pH, and reservoir

440 temperature followed by the rock site density. This specific finding highlights that injection water
 441 salinity is a key parameter to governing the prospects of low salinity waterflooding in sandstone
 442 reservoirs. Analysis shows that increasing the salinity from 0.1 to 3 M NaCl will result in the MEB
 443 reversing its sign from positive to negative, hence, shifting reservoir wettability from strong water-
 444 wet to weak or intermediate water-wet conditions. The results of these analyses also highlight the
 445 importance of rock mineralogy in dictating the overall reservoir wettability. By increasing the
 446 average rock site density from the base value 2.5 site/nm² to the maximum of 5.5 site/nm², which
 447 corresponds to the kaolinite clay site density (see Table 1), the film stability drastically drops 53%
 448 from its base value 0.47 mJ/m². Such finding indicates that the inclusion of mineralogy is essential
 449 in sandstone reservoir wettability prediction. Another interesting finding in our work is that the
 450 effect of oil composition change on the overall system stability is not as pronounced as the other
 451 parameters. Results show that changing the TAN of crude oil between a maximum and minimum
 452 of 0.01 and 3 mg KOH/g results in a maximum of 31% change in the energy barrier. While
 453 changing the TBN of a crude oil between 0 and 3 mg KOH/g results in a minimal less than 1% in
 454 the energy barrier. This observation suggests that the amounts of acidic polar compounds in the
 455 crude oil have a dominant effect over basic components to impact the wettability in sandstones.

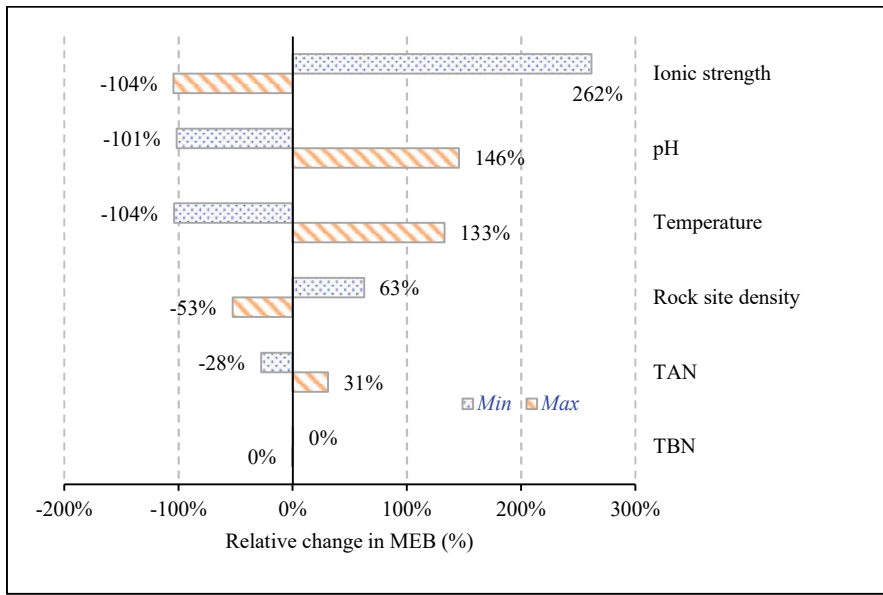
456 **Table 4 Ranges of the selected parameters for sensitivity analyses**

Parameter	Base	Min	Max	Maximum energy barrier (mJ/m ²)		
				Base	Min	Max
Ionic strength (M NaCl)	0.5	0.01	3	0.47	1.7	-0.02
pH	7	5	9	0.47	-0.0068	1.154
Temperature (°C)	60	25	100	0.47	-0.018	1.095
Rock site density (site/nm²)	5	1.2	11	0.47	0.764	0.223
TAN (mg KOH/g)	0.5	0.01	3	0.47	0.34	0.616
TBN (mg KOH/g)	0.5	0	3	0.47	0.472	0.469

457

458 We further employed our triple-layer model to evaluate the effect of continuous change of the
459 studied parameters on the overall oil-brine-sandstone system. Figure 10 compares the effects of
460 temperature and pH changes on the MEB using the base case values listed in Table 4. It can be
461 observed the increase in pH value results in a continuous increase in the energy barrier almost in a
462 linear manner (Figure 10a), which allows us to predict that an increase in pH will always result in
463 strengthening the water-wet conditions in sandstone reservoirs. This is one of the suggested
464 mechanisms of the low salinity waterflooding [7] which is also the underlying mechanism in
465 alkaline flooding. Figure 10b shows that an increase in the temperature between 25 and 100 °C, in
466 cases of using 0.5 and 1 M NaCl, results in an increase in the energy barrier from -0.02 mJ/m² to
467 0.53 mJ/m² and 1.0975 mJ/m², respectively. However, in the case of a 0.01 M NaCl background
468 electrolyte, the energy barrier increases from 0.695 mJ/m² to a maximum 1.75 mJ/m² at 80 °C
469 before dropping slightly to 1.6 mJ/m² at 100 °C. These results indicate that the pronounced effect
470 of temperature on reservoir wettability in low salinity waterflooding mostly takes place below 80
471 °C. It can also be concluded that the temperature increase beyond 80 °C - 100 °C may result in
472 reversing the wettability trend into less favourable conditions. This trend could be due to possible
473 surface overcharging, leading to a decrease in the negative surface charge and eventually reversing
474 the wettability [67].

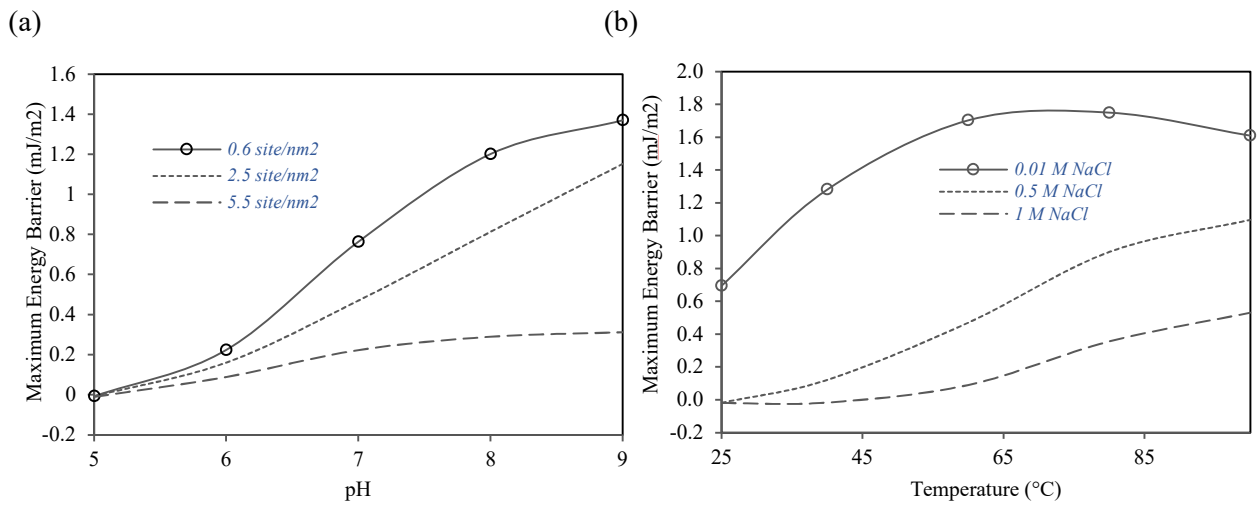
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Figure 9 Relative change of maximum energy barrier against the different parameters



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Figure 10 Sensitivity of maximum energy barrier against (a) pH at various average rock site densities and (b) temperature at various salinities

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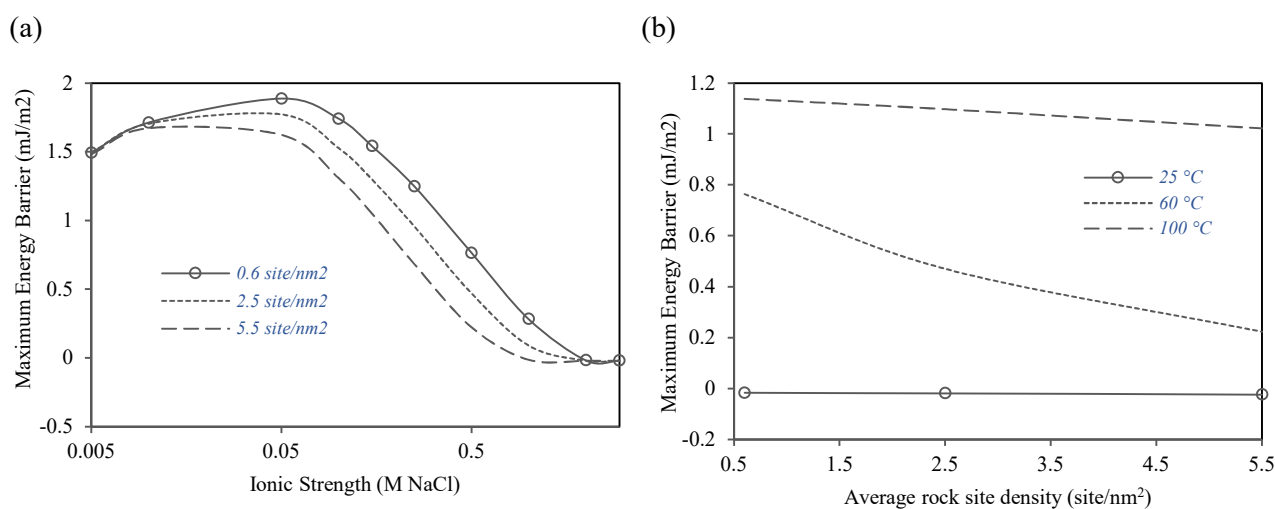
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The effects of the ionic strength and average rock site density on the MEB were calculated and the results are shown in Figure 11. It shows that the increase in ionic strength of NaCl from 0.005 M to 3 M at different rock site densities results in a reduction in the MEB. It can be noticed that the effect of ionic strength on the MEB is pronounced in the range between 0.05 and 2 M NaCl where the MEB drops from 1.77 to -0.02 mJ/m². The energy barrier drops below the zero value when the

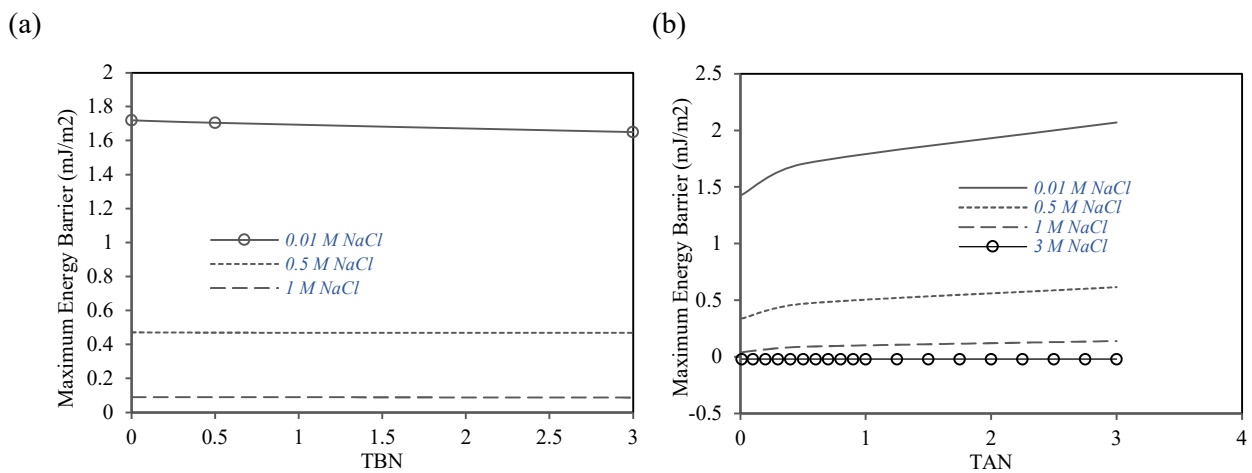
486 ionic strength increases beyond 2 M NaCl and stabilises at a maximum negative value of
 487 approximately -0.02 mJ/m^2 . This implies that the target of low salinity waterflooding in a case
 488 where a reservoir with the initial conditions such as shown in Table 4 and formation water of 2 M
 489 NaCl, would be to use the injection water with a salinity less than 1 M NaCl for observing the
 490 favorable effect. Figure 11b also shows that the increase in the average rock site density has a
 491 descending effect on the oil-brine-sandstone system which is specifically evident at temperatures
 492 higher than 25°C . A high average rock site density results in more sites being available for the
 493 cations present in the brine to adsorb and screen the negative charge present on the sandstone
 494 surface. Such less negative charge results in less repulsion between the rock surface and the
 495 negatively charged oil surface leading to more oil adherence to the rock surface. This is evident
 496 quantitatively in Figure 11b for the case of 60°C temperature where the increase of average rock
 497 site density from 0.6 to 5.5 site/nm^2 leads to a drop in the MEB from 0.764 mJ/m^2 to 0.224 mJ/m^2 ,
 498 shifting the wettability towards less water-wet conditions.



499
 500 **Figure 11 Sensitivity of maximum energy barrier against (a) ionic strength at various average rock**
 501 **site densities and (b) average rock site density at various temperatures**

502 The impact of oil polar compounds on the MEB are depicted in Figure 12. It can clearly be seen
 503 that the effect of TAN on the MEB is more pronounced compared to TBN. This can be attributed
 504 to the fact that the TBN and positively charged amines surface groups are more present at lower

505 pH values where an excess of hydrogen ions associates with (-NH) to create (-NH₂⁺). And because
 506 our studied range of pH is between 5 and 9, the effects of TBN and positively charged amine groups
 507 are not fully captured. Nevertheless, we can assume that the oil TBN does not have a pronounced
 508 effect under the usual reservoir conditions. TAN on the other hand does influence the oil-brine-
 509 sandstone system stability and wettability in reservoir conditions. Figure 12b shows that at lower
 510 salinities, an increase in the TAN results in an increase in the MEB. However, as the salinity
 511 increases and the concentration of the positive sodium ions available for adsorption increases, the
 512 increase in TAN results in a negligible change in the MEB. NaCl salinities above 1 M NaCl show
 513 a reversal in the trend where increasing the TAN leads to a very slight decrease in the MEB and
 514 hence the system stability.



515
 516 **Figure 12 Sensitivity of maximum energy barrier against (a) TBN and (b) TAN at various salinities**

517 **4.5 Wettability change with reservoir conditions**

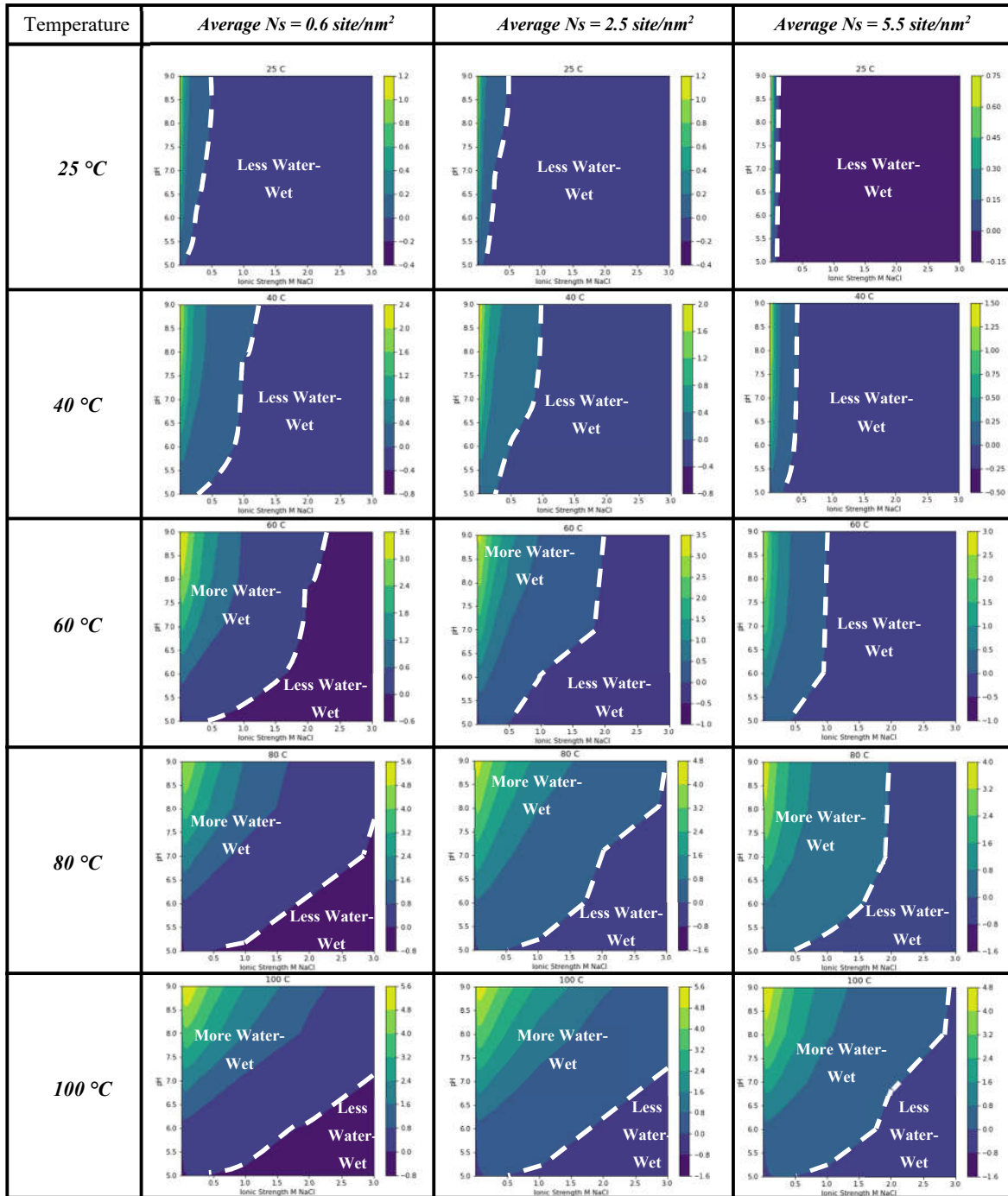
518 In this section, the approaches used in this study are combined to quantify and provide an indicative
 519 adhesion or wettability map under the variable reservoir properties and conditions. We focus our
 520 investigation on identifying the effects of the most impactful reservoir parameters on the oil-brine-
 521 sandstone stability and wettability: pH, ionic strength, average rock site density and temperature
 522 (as discussed in the previous sections). The evaluation range of each parameter is listed in Table 4.

523 The results of these analyses were combined and summarised as wettability maps as visualised in
524 Figure 13 and Figure 14.

525 *4.5.1 Wettability map for sandstone rock in NaCl*

526 Figure 13 shows the wettability map under the various combinations of reservoir properties and
527 using NaCl as the background electrolyte in the brine. It depicts the reservoir conditions that result
528 in negative MEB that indicates weak or intermediate wetting conditions. This map demonstrates
529 the importance of salinity in determining reservoir wettability. Under almost all conditions,
530 decreasing the brine salinity resulted in an increase in the strong water-wet conditions area in the
531 map, especially, when the average rock site density is lower where the salinity effect is more
532 pronounced. This demonstrates that the main focus of LSWF in sandstone reservoirs should involve
533 reducing the brine ionic strength, which can result in shifting the reservoir wettability from
534 weak/intermediate water-wet to strongly water-wet. Another important observation is the crucial
535 role the average rock site density and clay mineralogy play in dictating the reservoir wettability.
536 The map in Figure 13 shows that having a higher site density such as 5.5 site/nm² causes the
537 reservoir to become weak water-wet over a wide range of reservoir conditions. This observation
538 highlights the importance of rock mineralogy in terms of composition and clay content and
539 appropriately modelling it in wettability predictions.

540 The wettability map also shows that the increase in temperature from 25 to 100 °C moves the
541 reservoir wettability towards more wetting conditions within the studied range of parameters.
542 Hence, indicating that hot low salinity waterflooding would be more beneficial under certain
543 reservoir conditions.



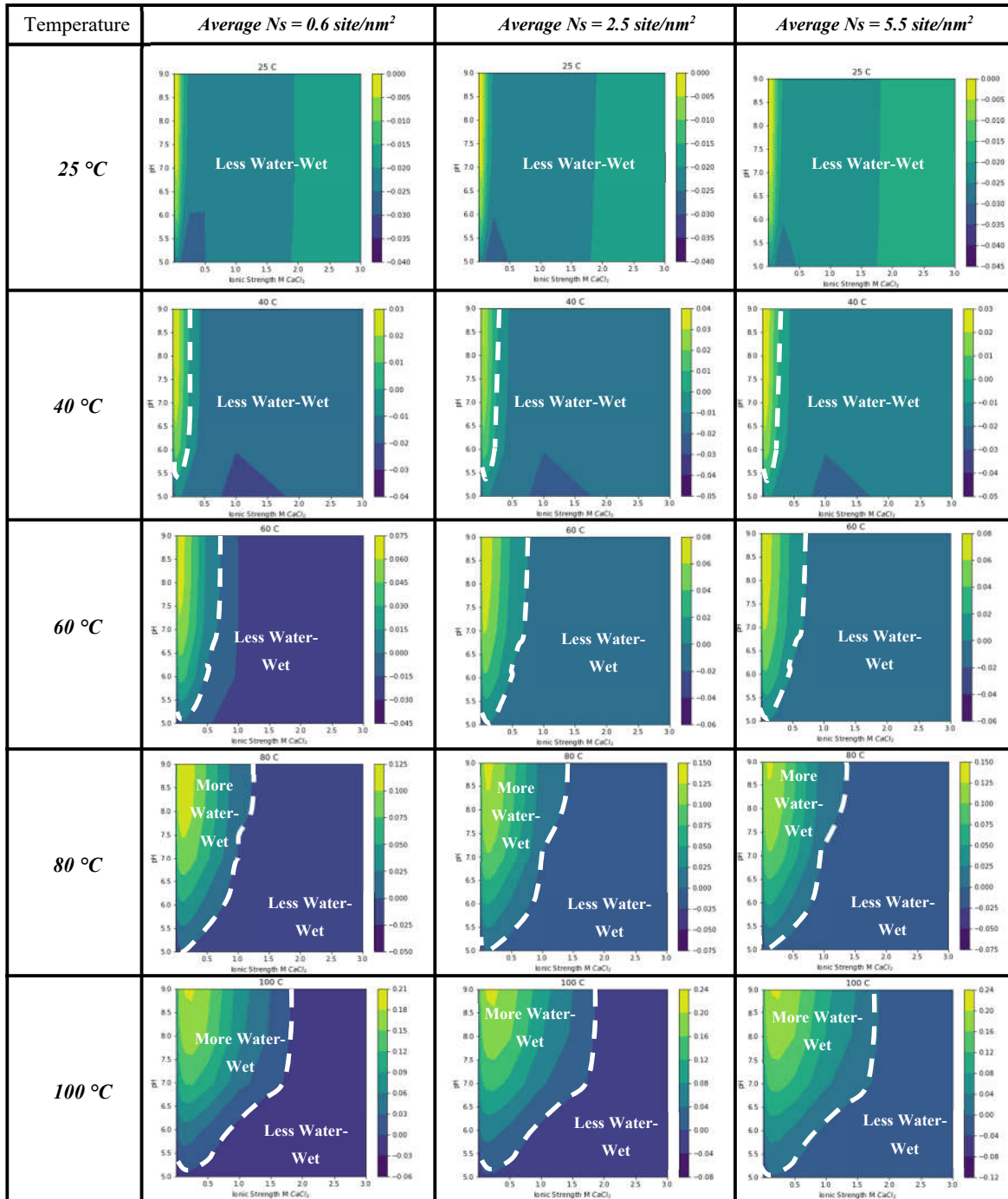
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545 **Figure 13 Wettability map against NaCl ionic strength, pH, temperature, and average rock site**
 546 **density**

547 *4.5.2 Wettability map for sandstone rock in CaCl₂*

548 The same wettability map approach was used to evaluate the influence of the divalent cations such
 549 as Ca²⁺ in the formation brine on the reservoir wettability. The same ranges listed in Table 4 for

550 the rest of the reservoir parameters are used. The wettability map in Figure 14, demonstrates how
551 impactful the presence of the calcium ion is on the reservoir wettability in comparison with the
552 monovalent sodium ion (see Figure 13). The strong water-wet area in the adhesion map (Figure 14)
553 increases as the pH and temperature values increase which enhance the deprotonation of surface
554 sites leading to higher negative surface charge and repulsion between the two surfaces. The increase
555 in the average rock surface site density from 0.6 to 5.5 site/nm² suppresses the strong water-wet
556 area in the adhesion map. This can be attributed to the increase in the available surface sites for the
557 positive Ca²⁺ ions to adsorb on and screen the negative charge present at the rock surface.
558 Overall, the presence of the calcium ion significantly suppresses the areas of strong water
559 wettability under different conditions. Such finding is directly linked with the way how the calcium
560 ion affects the zeta potential at sandstone and oil-brine interfaces. Adsorption of Ca²⁺ greatly
561 reduces the negative values of the zeta potential and surface charge in comparison to sodium ion
562 thereby resulting in less electrostatic repulsion between the two interfaces. As a result, significant
563 low salinity effect and wettability alteration are expected if low salinity NaCl brine is injected into
564 sandstone reservoirs comprising of calcium-rich formation water.



565

566

Figure 14 Wettability map against CaCl_2 ionic strength, pH, temperature, and average rock site

567

density

568 5 Summary and Conclusions

569

A new sandstone-brine triple-layer surface complexation model was developed and validated

570

against results from the published experimental studies. The developed model is the first to

571

accommodate the individual and combined effects of sandstone minerals on the overall zeta

572 potential. The stability of the COBR system was analysed by calculating the disjoining pressure
573 and interaction potential energy between the COBR interfaces using the DLVO. Furthermore, we
574 introduced a new maximum energy barrier (MEB) concept as an indicator of reservoir wettability.
575 The MEB was correlated well with contact angle measurements from the reported experimental
576 studies. Analysis of the results showed that the contact angle value increases abruptly as the MEB
577 drops below the zero-value indicating that the COBR system becomes unstable and less water-wet.
578 This finding validates the application of maximum energy barrier concept (maximum of the
579 interaction potential energy curve) to characterise reservoir wettability as a function of brine, oil
580 and rock compositions, and reservoir conditions.

581 The developed TLM and MEB parameters were utilised to analyse the effect of sandstone
582 mineralogy on the rock-brine zeta potential and reservoir wettability. The presence of kaolinite in
583 the sandstone reservoir causes the COBR system to become less stable and less water-wet in
584 comparison with the other studied clay minerals i.e. chlorite, illite, montmorillonite and smectite.
585 Further sensitivity analysis indicated that the brine composition is the most impacting parameter
586 on reservoir wettability amongst the investigated parameters. The importance of different studied
587 parameters on reservoir wettability in sandstones was found to be in the following order: ionic
588 strength and brine composition > pH > temperature > sandstone mineralogy > oil TAN > oil TBN.
589 Furthermore, the rapid change in the maximum energy curve with the average rock site density
590 demonstrates the significance of the sandstone rock mineralogy in dictating the wettability of the
591 oil-brine-sandstone system. Also, the presence of CaCl_2 in the formation water significantly
592 suppresses the areas of strong water wettability under different reservoir conditions compared to
593 NaCl.

594 The modelling work conducted in this research is limited to the types of clay considered in the
595 sandstone-brine triple-layer model i.e. kaolinite, chlorite, illite, montmorillonite and smectite.
596 Other clays and minerals may also be present in a sandstone rock. Moreover, the validation range

597 of the data used for optimising the developed oil-brine and sandstone-brine models is between 50
 598 and 175,000 ppm for brine salinity, between 25 and 65 °C for temperatures and 2 – 11 pH. The
 599 application of the developed workflow was also extended outside these validation ranges to gain
 600 valuable insights into how these different parameters affect sandstone wettability. Nonetheless, the
 601 workflow presented in this study will provide useful practical guidelines in screening sandstone
 602 reservoir candidates for potential low salinity waterflooding applications.

603 **6 Abbreviations and Nomenclature**

604 **6.1 Abbreviations**

CD-MUSIC	Charge-distribution multisite surface complexation
COBR	Crude oil-brine-rock
DLVO	Derjaguin, Landau, Verwey, and Overbeek
LSE	Low salinity effect
LSWF	Low salinity waterflooding
MEB	Maximum energy barrier
MIE	Multicomponent ion exchange
PDI	Potential determining ions
SCM	Surface complexation modelling
TAN	Total acid number
TBN	Total base number
TLM	Triple-layer surface complexation models

VdW

Van der Waal

605

606 **6.2 Nomenclature**

A

Hamaker constant

$A_{v=0}, A_{v>0}$

Contributions to Hamaker constant at zero and finite frequencies

A_s

Structural force coefficient

C_1, C_2

Capacitances of the inner and outer Helmholtz layers

d

Thickness of the layer

e

Electron charge

F

Faraday constant

h

Distance between the two interfaces

I

Ionic strength of the solution

k_B

Boltzmann constant

MW_{KOH}

Molecular weight of KOH

n_1, n_2, n_3

Refractive indexes for medium 1, 2, 3

N_A

Avogadro's number

n_b

Ion density in the bulk solution

N_s

Surface site density

T

Temperature

x

Distance away from the surface in meters

ϵ_0

Dielectric constant of free space

ϵ

Relative dielectric constant

ζ

Zeta potential

κ	Debye-Huckel parameter
λ_{lw}	London wavelength
$\Pi(h)$	Disjoining pressure
$\Pi_{electric}(h)$	Electrostatic forces
$\Pi_{structural}(h)$	Structural forces
$\Pi_{vdw}(h)$	Van der Waals forces
ρ	Ionic concentration
σ	Charge density
ψ	Potential
ψ_r	Reduced surface potential

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